



# Magnetically recyclable Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> microspheres for effective removal of Congo red dye by simultaneous adsorption and photocatalytic regeneration



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## ABSTRACT

Novel magnetic bayberry-like Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> microspheres (Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs) combining highly effective adsorption and photocatalytic regeneration were prepared by a facile hydrothermal method. The resultant Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs were characterized by XRD, SEM, EDS, VSM, BET and DRS. Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs possessed a relative large surface area of 36.0 m<sup>2</sup> g<sup>-1</sup> and narrow pore size distribution around 4.72 nm. The equilibrium and kinetics of adsorption process followed the Langmuir isotherm model and pseudo-second-order kinetic model, respectively. Maximum adsorption capacity of CR as 92.24 mg g<sup>-1</sup> was achieved on Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs, while only 66.28 mg g<sup>-1</sup> was found on Bi<sub>2</sub>S<sub>3</sub> MSs. High saturation magnetization, low coercivity and remnant magnetization values of Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs indicated that easy separation and fast re-dispersion in aqueous solution can be realized. What's more important, Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs with a stronger absorption in the visible light region can be regenerated by photocatalysis under simulated solar light irradiation. Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs also showed excellent stability and reusability for continuous removal of Congo red dye by synergistic adsorption and photocatalytic regeneration. As a result, Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs provided effective and conveniently recyclable materials for environmental remediation by means of providing the facile preparation, easy magnetic separation, high adsorption, and simple regeneration.

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## 1. Introduction

According to the Colour Index, over 10,000 types of dyes are being manufactured, and annual worldwide dye production is more than 700,000 tons. It is estimated that about 10% of dyes used in industry are finally discharged into the aqueous environment, which is quite harmful to the human health and aquatic ecosystem due to their high carcinogenicity and toxicity [1]. For effective removal of those dyes from industrial wastewater, various techniques, including adsorption [2,3], flocculation-coagulation [4], ozonation [5], sonocatalysis [6], and photocatalysis [7–9], have been developed recently. Among those approaches, synergistic method of adsorption and photocatalysis has been shown to be an effective method to treat containing-dye wastewater [8–13].

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As a direct band gap material with a gap energy (E<sub>g</sub>) of 1.3 eV, bismuth sulfide (Bi<sub>2</sub>S<sub>3</sub>) has drawn intensive attention for its potential applications in photocatalysis [14–16], electrochemical applications [17–19], photodetector [20,21], environmental remediation [22–24], and solar energy conversion [25,26]. Recently, many Bi<sub>2</sub>S<sub>3</sub>-based nanocomposites, such as SiO<sub>2</sub>/Bi<sub>2</sub>S<sub>3</sub> [27], BiVO<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> [14], Bi<sub>2</sub>S<sub>3</sub>/In<sub>2</sub>S<sub>3</sub> [28], Bi<sub>2</sub>S<sub>3</sub>-BiOCl [29], CuS/Bi<sub>2</sub>S<sub>3</sub> [30], Bi<sub>2</sub>S<sub>3</sub>/Bi<sub>2</sub>SiO<sub>5</sub> [31], Bi<sub>2</sub>S<sub>3</sub>/g-C<sub>3</sub>N<sub>4</sub> [22], and Bi<sub>2</sub>S<sub>3</sub>/Bi<sub>2</sub>WO<sub>6</sub> [16], have been successfully fabricated by different techniques, and their novel and unique adsorption and photocatalytic properties have been extensively explored. Those studies have demonstrated that Bi<sub>2</sub>S<sub>3</sub>-based nanocomposites possess excellent photocatalytic performance for eliminating various toxic organic pollutants [22,23,27,28]. However, because of their small sizes, easy recovery and continuous reusability of Bi<sub>2</sub>S<sub>3</sub>-based nanocomposites are still a challenge in practical treatment system.

The separation and recovery of nanomaterials from solution with the use of magnetic fields is more selective, efficient and faster than centrifugation or filtration [32]. Magnetically recyclable

materials has become an active and important field of corresponding researches [33–35]. Some magnetic chemicals have been used as the magnetic carriers, such as  $\text{Fe}_3\text{O}_4$  [32,36–38],  $\gamma\text{-Fe}_2\text{O}_3$  [9,35] and  $\text{MFe}_2\text{O}_4$  ( $\text{M} = \text{Ni}, \text{Co}, \text{Zn}, \text{Cu}$ ) [13,39], to prepare all kinds of magnetic nanocomposites. Among them,  $\text{Fe}_3\text{O}_4$  nanoparticles with good magnetic response can accomplish the simple magnetic separation and recovery of suspended nanocomposites using an external magnet [37,40,41]. In addition, the excellent adsorption ability of  $\text{Fe}_3\text{O}_4$  nanoparticles with high specific surface area to pollutant molecules is also conducive to effective removal of organic pollutants [42]. Recently, various types of  $\text{Fe}_3\text{O}_4$ /semiconductor nanocomposites, such as  $\text{Fe}_3\text{O}_4/\text{BiOI}$  [40],  $\text{Fe}_3\text{O}_4/\text{SiO}_2/\text{BiOBr}$  [43],  $\text{ZnO-Fe}_3\text{O}_4$  [42,44],  $\text{ZnO-Fe}_3\text{O}_4/\text{SiO}_2$  [45],  $\text{Fe}_3\text{O}_4/\text{AgBr}$  [46],  $\text{Fe}_3\text{O}_4/\text{CuO}$  [41], and  $\text{Fe}_3\text{O}_4/\text{TiO}_2$  [37] have been synthesized. However, to the best of our knowledge, less research has been done on the facile synthesis and characterization of magnetically recyclable  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  microspheres ( $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs) and their application of synergistic adsorption and photocatalysis in removal of dyes under simulated solar light irradiation.

Herein, magnetic bayberry-like  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were prepared using  $\text{Fe}_3\text{O}_4$  nanoparticles as magnetic resource and  $\text{Bi}_2\text{S}_3$  microspheres ( $\text{Bi}_2\text{S}_3$  MSs) as main adsorbent and photocatalyst by a facile hydrothermal method.  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were characterized by XRD, SEM, EDS, VSM, BET and DRS. The adsorption of magnetic bayberry-like  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were evaluated via the decolorization of Congo red (abbreviated as CR, chosen as a model pollutant). Adsorption kinetics and adsorption isotherms were applied to describe the CR adsorption process on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs. In addition, reusability of magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were examined by simultaneous adsorption and photocatalytic regeneration under simulated solar light irradiation. This information may be useful for further application of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs in removal of hazardous azo dyes from aqueous solution.

## 2. Materials and methods

### 2.1. Materials

$\text{Bi}(\text{NO}_3)_3 \cdot 5\text{H}_2\text{O}$ ,  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ ,  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ ,  $\text{NH}_3 \cdot \text{H}_2\text{O}$  (28%, v/v), thiocarbamide were purchased from Shanghai Chemical Reagents Research Institute (Shanghai, China) and used without further purification. Congo red (CR) used as model dye was purchased from Yongjia Fine Chemical Factory (Wenzhou, China).

### 2.2. Preparation of $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$ MSs

Firstly,  $\text{Fe}_3\text{O}_4$  nanoparticles were synthesized by coprecipitation of ferric and ferrous salts under the presence of  $\text{N}_2$  gas according to our previous literature [3]. Secondly, after 0.04 mol of thiocarbamide was dissolved completely into 50 mL of distilled water, 4 mmol of  $\text{Bi}(\text{NO}_3)_3 \cdot 5\text{H}_2\text{O}$  and 0.928 g of as-prepared  $\text{Fe}_3\text{O}_4$  nanoparticles were added in and stirred for 30 min and the solution was then transferred to a Teflon-lined stainless steel autoclave. The autoclave was sealed and maintained at 90 °C for 12 h and then cooled down to room temperature naturally. The precipitate was collected by a permanent magnet, washed several times with deionized water and ethanol, respectively, and dried at 80 °C till constant weight. For comparison, pure  $\text{Bi}_2\text{S}_3$  microspheres ( $\text{Bi}_2\text{S}_3$  MSs) also were synthesized using a revised solvothermal method [47,48].

### 2.3. Characterization of $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$ MSs

X-ray powder diffraction (XRD) analysis was performed on a Bruker AXS D8-advance X-ray diffractometer at 40 kV and 50 mA

with Cu target and  $\text{K}\alpha$  radiation ( $\lambda = 0.154 \text{ nm}$ ) in the range of  $2\theta$  from 10° to 70°. UV–vis diffuse reflectance spectra (UV–vis DRS) of the samples were obtained by using an UV-3100 UV–vis spectrophotometer (Hitachi Corporation, Japan).  $\text{BaSO}_4$  was used as a reflectance standard in UV–vis diffuse reflectance experiment. The morphology and elemental composition of the synthesized samples were characterized by energy-dispersive X-ray spectroscopy with a scanning electron microscope (SEM, Hitachi S4800 equipped with an EDS). Nitrogen gas porosimetry measurement was obtained using a MPMS-XL-7 surface area and porosity analyzer (Quantum Design, America). VSM measurements were performed by using a MPM5-XL-5 superconducting quantum interference device (SQUID) magnetometer. The magnetization measurements were carried out in an external field up to 10 kOe at room temperature (293 K).

### 2.4. Evaluation of adsorption performance

Dye adsorption experiments were performed on a model KYC-1102 C thermostat shaker (Ningbo, China). Stock solutions of CR ( $1000 \text{ mg L}^{-1}$ ) were prepared by dissolving 1 g of CR in 1000 mL double distilled water. To carry out adsorption experiments, 0.02 g of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was added to 50 mL of CR aqueous solution with a fixed concentration under stirring at room temperature. At predetermined time intervals, about 5 mL aliquots were sampled and separated by a magnet. The remaining concentration of CR in supernatant solution was determined by using a TU 1810 UV–visible spectrophotometer (Beijing Purkinje General Instrument Co., Ltd, China). The amount of adsorption  $q_t$  ( $\text{mg g}^{-1}$ ) and the decolorization efficiency  $\eta$  (%) can be calculated according to Eqs. (1) and (2), respectively.

$$q_t = \frac{(C_0 - C_t) \times V}{m} \quad (1)$$

$$\eta = \frac{(C_0 - C_t)}{C_t} \times 100\% \quad (2)$$

where  $q_t$  ( $\text{mg g}^{-1}$ ) is the amount adsorbed per gram of adsorbent at time  $t$  (min),  $C_0$  is the initial concentration of CR in the solution ( $\text{mg L}^{-1}$ ),  $C_t$  is the instant concentration of CR at time  $t$  of adsorption ( $\text{mg L}^{-1}$ ),  $m$  is the mass of the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs (g), and  $V$  is the volume of solution (L).

### 2.5. Photocatalytic recycling under simulated solar light irradiation

The photocatalytic recycling of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was performed in a photochemical reactor (Nanjing Xujiang Electromechanical Factory, Nanjing, China) under simulated solar light irradiation. A 300 W xenon lamp was used as a simulated solar light source, which was positioned in the cylindrical quartz trap at ambient temperature controlled by a water-cooling system. In a typical experiment, 20 mg of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was dispersed into a 50 mL of CR solution ( $30 \text{ mg L}^{-1}$ ). Then, the dispersion was exposed to simulated solar light irradiation. During reaction, the resulting aqueous suspension containing CR and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was continuously stirred and bubbled so that the concentration of dissolved oxygen in reaction system was kept constant. At given time intervals, 5 mL of dispersion was drawn and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were separated immediately by an ordinary magnet. Residual CR concentration in supernatant was analyzed at  $\lambda_{\text{max}} = 496.0 \text{ nm}$  using a TU 1810 UV–visible spectrophotometer (Beijing Purkinje General Instrument Co., Ltd, China). Removal efficiency ( $\eta$ ) of CR solution by  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs at time  $t$  can be calculated by Eq. (2).

### 3. Results and discussion

#### 3.1. Characterization of materials

##### 3.1.1. XRD analysis and UV–vis diffuse reflectance spectra

Fig. 1a represents XRD patterns of pure  $\text{Fe}_3\text{O}_4$ ,  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs. It can be easily found that the diffraction peaks of pure  $\text{Fe}_3\text{O}_4$  at  $2\theta = 30.32^\circ$ ,  $35.64^\circ$ ,  $43.36^\circ$ ,  $53.66^\circ$ ,  $57.26^\circ$  and  $62.87^\circ$  match the reflections of (220), (311), (400), (422), (511) and (440), respectively, indexed to the cubic spinel structure of  $\text{Fe}_3\text{O}_4$  (JCPDS 56-3107) (Fig. 1a) [44]. All of the diffraction peaks of  $\text{Bi}_2\text{S}_3$  MSs are in good accordance with the standard card of orthorhombic  $\text{Bi}_2\text{S}_3$  (JCPDS 75-1306) [17]. The pattern of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs exhibit a coexistence of the  $\text{Fe}_3\text{O}_4$  and  $\text{Bi}_2\text{S}_3$ , indicating the formation of the nanocomposites. No additional phases are evident found from the XRD patterns of all samples. The crystalline sizes of  $\text{Fe}_3\text{O}_4$  and  $\text{Bi}_2\text{S}_3$ , determined by the Debye–Scherrer equation [40], were found to be 9 and 4 nm, respectively. Yavuz's research showed that 8–12 nm-size represents the optimal size for magnetic separations [32], which is further demonstrated below by VSM studies.

Fig. 1b displays the UV–vis diffuse reflectance spectra (DRS) of  $\text{Fe}_3\text{O}_4$ ,  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs. It is worth noting that  $\text{Bi}_2\text{S}_3$  MSs have strong absorption over the whole visible light region [14,29]. The band gap of pure  $\text{Bi}_2\text{S}_3$  is about 1.3 eV [22]. Pure  $\text{Fe}_3\text{O}_4$  has photo-absorption not only in UV light range, but also in visible light range. However, light absorption of  $\text{Fe}_3\text{O}_4$  weakens with increasing wavelength in the range of visible light. The whole light absorption ability of the  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs increased obviously with the introduction of  $\text{Bi}_2\text{S}_3$ , which should be attributed to the small band gap and large absorption coefficient of  $\text{Bi}_2\text{S}_3$  [49]. Compared with the magnetic photocatalysts reported in literatures [29,43,44],  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs have strong absorption in the UV–visible-light region from 200 to 800 nm, implying it possible to regenerate the materials by photocatalysis under simulated solar light irradiation after  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs have adsorbed targeted pollutants.

##### 3.1.2. Morphology and microstructure

The surface morphology, microstructure and sizes of  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were determined by SEM. Fig. 2a shows the low-magnification SEM image of  $\text{Bi}_2\text{S}_3$  MSs by hydrothermal method using thiocarbamide as sulfur source. It reveals that  $\text{Bi}_2\text{S}_3$  MSs consisted of bayberry-like microspheres with diameters in

the range of 1.3–4.5  $\mu\text{m}$  [50]. The high magnified SEM image of  $\text{Bi}_2\text{S}_3$  MSs shows that individual  $\text{Bi}_2\text{S}_3$  microsphere was constructed with nanorods (Fig. 2b). The  $\text{Bi}_2\text{S}_3$  nanorods grew from the center of the microsphere, resulting in the formation of a hierarchical bayberry-like  $\text{Bi}_2\text{S}_3$  microsphere [30]. With the introduction of ferroferric oxide ( $\text{Fe}_3\text{O}_4$ ), bayberry-like structure of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs with an average size of 2.0  $\mu\text{m}$  still could be easily obtained (Fig. 2c), and its surface is made up by thin  $\text{Bi}_2\text{S}_3$  nanorods and  $\text{Fe}_3\text{O}_4$  nanoparticles (Fig. 2d). It's worth noting that not all  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs presented perfectly spherical and their surface are more uneven than those of  $\text{Bi}_2\text{S}_3$  MSs (Fig. 2d), indicating that the presence of  $\text{Fe}_3\text{O}_4$  nanoparticles disturbed the growth of the  $\text{Bi}_2\text{S}_3$  crystal to some extent. The compositions of different locations on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were determined by X-ray energy-dispersive spectroscopy (EDS), as shown in Fig. 2e and f. The EDS analysis of the surface showed peaks for Bi and S, as well for Fe and O, which reveal the implantation of the  $\text{Fe}_3\text{O}_4$  in the  $\text{Bi}_2\text{S}_3$  nanorods. However, there is no iron element in the interior of the microsphere, which indicated that a bayberry-like structure of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was not grown directly on the  $\text{Fe}_3\text{O}_4$  surface.

##### 3.1.3. Vibrating sample magnetometer

The magnetic properties of  $\text{Fe}_3\text{O}_4$  and as-prepared  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were measured and the corresponding results are shown in Fig. 3. The saturated magnetization of pure  $\text{Fe}_3\text{O}_4$  nanoparticles was  $66.50 \text{ emu g}^{-1}$ , which is consistent with those reported in the literature [36,51]. However, the saturated magnetization of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs reduced to  $18.80 \text{ emu g}^{-1}$  with the introduction of bismuth sulfide, which is still higher than the values of other reported magnetic material, such as  $\text{ZnO–Fe}_3\text{O}_4/\text{SiO}_2$  [45] and  $\text{Fe}_3\text{O}_4/\text{ZnO}$  [44]. The acceptable saturation magnetization value indicated that as-prepared  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were suited to easy magnetic separation. After adding an external magnetic field, complete magnetic separation of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was achieved in 30 s by a permanent magnet near the wild-mouth bottle (Fig. 3b). The coercivity and remanent magnetization values are about 13.70 Oe and  $0.65 \text{ emu g}^{-1}$  for  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs, respectively. The coercivity of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs at room temperature is almost negligible, indicating the ferrimagnetic and superparamagnetic property of as-prepared  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs [51]. Once the permanent magnet was removed, the  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs could be easily re-dispersed in aqueous solution by a slight agitation or ultrasound, demonstrating that easy, fast separation and redispersion of the  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs can be realized in aqueous solution. Combined with the other unique

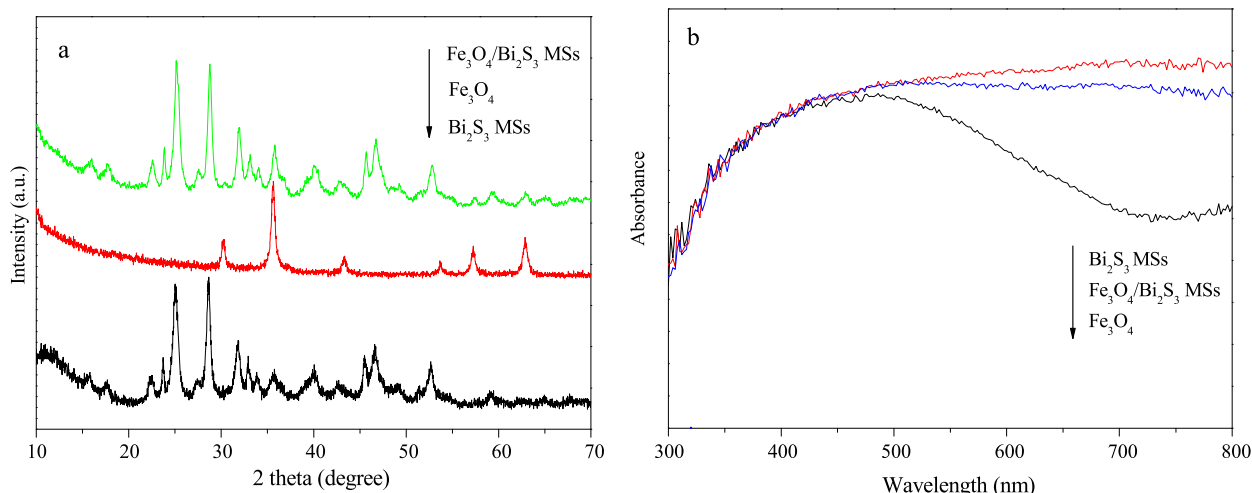


Fig. 1. XRD patterns (a) and UV–vis absorption spectra (b) of pure  $\text{Fe}_3\text{O}_4$ ,  $\text{Bi}_2\text{S}_3$  MSs, and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs.

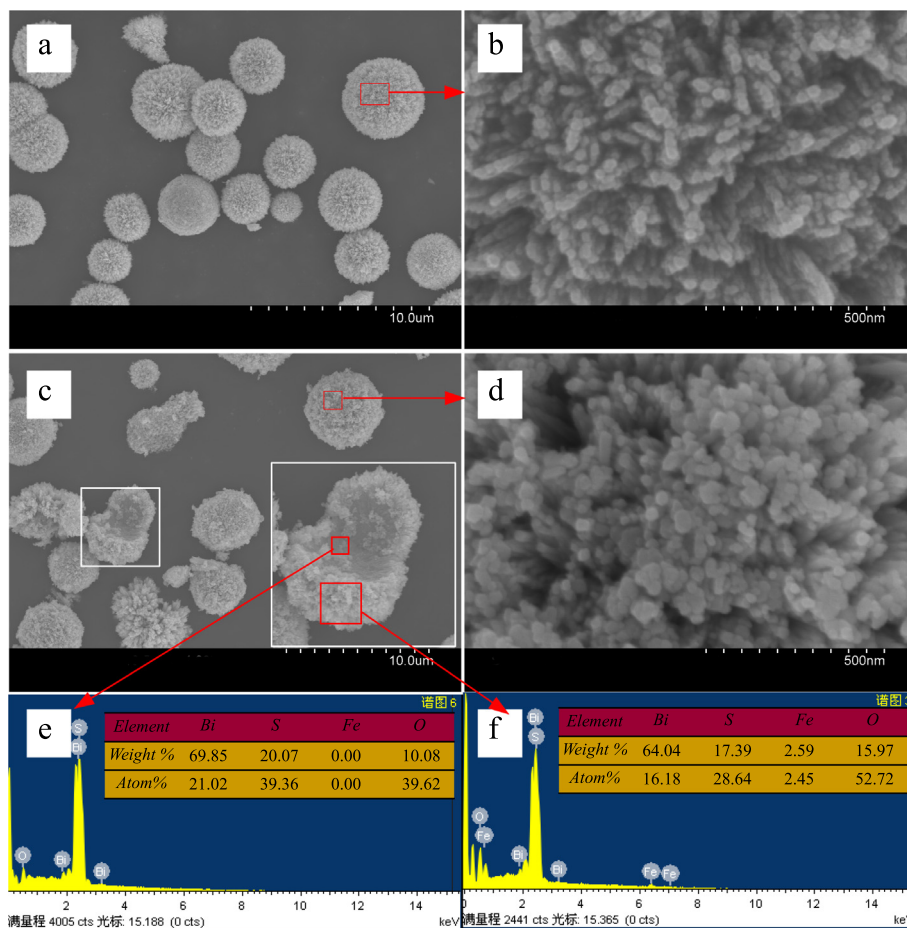


Fig. 2. SEM images of the  $\text{Bi}_2\text{S}_3$  MSs (a, b) and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs (c, d) and EDS spectrum (e, f) of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs.

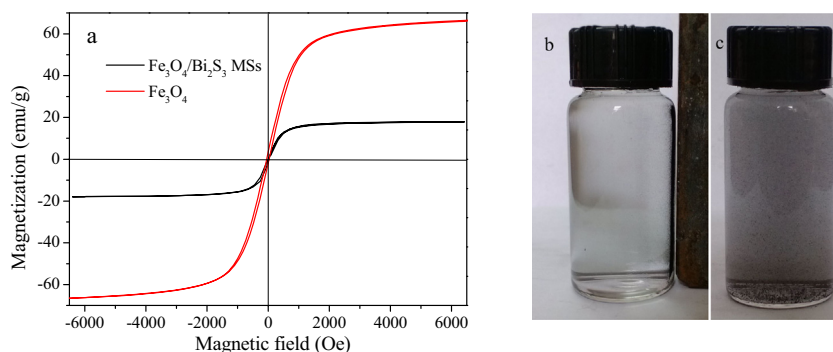


Fig. 3. Hysteresis loops curves of  $\text{Fe}_3\text{O}_4$  and the as-prepared  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs (a) at 293 K (a), magnetic separation of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs using an external magnet (b) and the redispersion of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs (c).

properties, the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs can be explored as a potential material in wastewater treatment without secondary pollution for water treatment.

### 3.1.4. $\text{N}_2$ adsorption–desorption isotherms

To give further insight into the physical structure, Brunauer–Emmet–Teller (BET) specific surface areas and the pore size distributions of  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were determined by nitrogen adsorption–desorption measurement and the results are shown in Fig. 4. As shown in Fig. 4a, the  $\text{N}_2$  adsorption–desorption isotherm of both  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs exhibit type IV, indicating the existence of abundant mesoporous

structures in those microspheres [39]. A broad hysteresis loop in the relative pressure range from 0.46 to 0.96 is reported for materials comprised of aggregates (loose assemblages) of particles forming slit like pores [52]. Compared with a BET surface area of  $\text{Bi}_2\text{S}_3$  MSs ( $10.8 \text{ m}^2 \text{ g}^{-1}$ ), the obtained  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs possess a relative large surface area of  $36.0 \text{ m}^2 \text{ g}^{-1}$ . The average pore radius of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs is 4.72 nm, which is less than that of the as-obtained  $\text{Bi}_2\text{S}_3$  MSs (5.36 nm) (Fig. 5b). The high specific surface areas and mesoporous channels of magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs would be both favorable for improving adsorption capability and can be employed for dye-containing wastewater treatment.



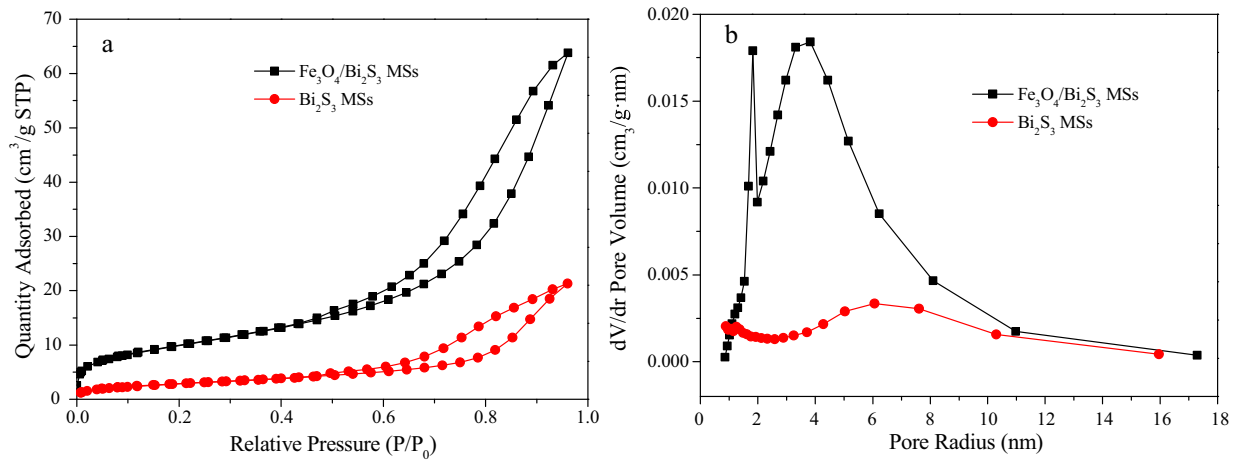


Fig. 4. Nitrogen adsorption–desorption isotherms (a) and pore-size distribution (b) of the  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs.

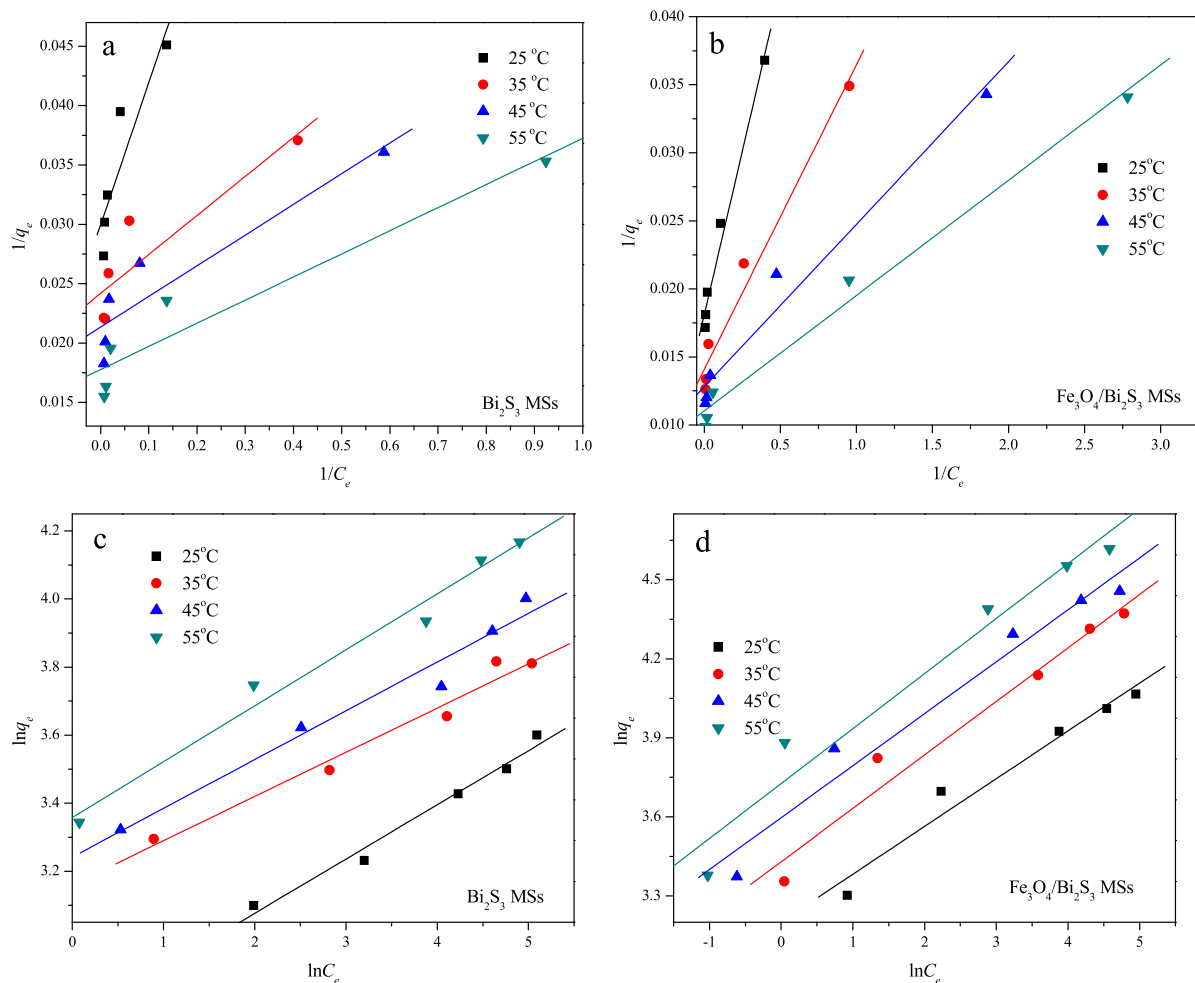


Fig. 5. Langmuir isotherms (a, b) and Freundlich isotherms (c, d) for CR adsorption on  $\text{Bi}_2\text{S}_3$  MSs and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs.

### 3.2. Adsorption isotherms

Adsorption isotherm is one of important data to explain the adsorption mechanism of contaminant on novel nanocomposite [27]. In addition, the adsorption of dye on nanocomposites is an important prerequisite for a synergistic adsorption-photocatalytic degradation process [8]. Therefore, Langmuir and Freundlich isotherm models were used to analyze the equilibrium adsorption

characteristics for CR dye on  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs. Langmuir and Freundlich equations is represented for Eqs. (3) and (4), respectively [3].

$$\frac{c_e}{q_e} = \frac{1}{bq_m} + \frac{c_e}{q_m} \quad (3)$$

$$\ln q_e = \ln K_F + \frac{1}{n} \ln c_e \quad (4)$$

where  $c_e$  ( $\text{mg L}^{-1}$ ) is equilibrium concentration of CR in solution,  $q_e$  ( $\text{mg g}^{-1}$ ) is the adsorption capacity of CR adsorbed at equilibrium,  $q_m$  ( $\text{mg g}^{-1}$ ) is maximum amounts of CR adsorbed per unit mass of adsorbent required for monolayer coverage of the surface,  $b$  ( $\text{L mg}^{-1}$ ) is a constant related to the heat of adsorption. The slope and intercept of linear plots of  $c_e/q_e$  against  $c_e$  yield the values of  $1/q_m$  and  $1/bq_m$  for Eq. (3).  $K_F$  ( $\text{mg}^{1-(1/n)} \text{L}^{1/n} \text{g}^{-1}$ ) is related to the adsorption capacity of the adsorbent and  $1/n$  is another constant related to the surface heterogeneity. The slope and intercept of linear plots of  $\ln q_e$  against  $\ln c_e$  yield the values of  $1/n$  and  $\ln K_F$  for Eq. (4).

Fig. 5 shows the isotherms of CR adsorption on  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs, while their maximum adsorption capacities ( $q_m$ ) and some theoretical parameters ( $q_m$ ,  $b$ ,  $K_F$ ,  $n$ , and  $R^2$ ) are summarized in Table 1. It was notable that an increase in temperature resulted in a corresponding increase in adsorption capacity of CR on both  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs, which showed that the adsorptions of CR onto  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs are endothermic process. In general, the Langmuir isotherm model describes monolayer adsorption process while the Freundlich isotherm model describes the adsorption on heterogeneous surfaces associated with several adsorbent–adsorbate interactions [27]. For the CR adsorption on  $\text{Bi}_2\text{S}_3$  MSs, the  $R^2$  values ( $R^2 > 0.968$ ) from the Freundlich equation (Eq. (4)) were all higher than those ( $R^2 < 0.890$ ) from the Langmuir model (Eq. (3)), which is responsible for the observed multilayer adsorption. However, for the CR adsorption on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs, the Langmuir equation represented the adsorption process and all  $R^2$  values were higher than 0.972, indicating that monolayer coverage of the dye adsorbed on the surface of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs. With the introduction of  $\text{Fe}_3\text{O}_4$ , magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs have bayberry-like structures, rough and porous surfaces and exposed more adsorption sites. As a result, the adsorption of CR on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs presents monolayer adsorption process. This result is in good agreement with the observations in SEM and BET analysis of  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs.

Table 2 compares the adsorption capacity of the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs with the other reported inorganic adsorbents. The maximum adsorption capacity of the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs towards CR is  $92.24 \text{ mg g}^{-1}$ , which is higher than those of adsorbents reported earlier, such as  $\text{Fe}_{3-x}\text{La}_x\text{O}_4$  ferrite [53],  $\text{Zn-Fe}_2\text{O}_4$  [54], Ca-bentonite [55], chitosan coated magnetic  $\text{Fe}_3\text{O}_4$  particle [56], activated carbon [57]. It is worth mentioning that the maximum adsorption capacity ( $92.24 \text{ mg g}^{-1}$ ) of CR on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was almost 12.76 times higher than that of the reported activated carbon ( $6.7 \text{ mg g}^{-1}$ ) [57]. Therefore,  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs are suitable and promising for CR removal from aqueous solutions since it has a relatively high adsorption capacity and easy magnetic separation.

### 3.3. Effect of initial CR concentration on adsorption

Fig. 6 presents the time-dependent adsorption performance of the  $\text{Bi}_2\text{S}_3$  MSs and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs towards the removal of CR at different initial dye concentrations in aqueous solutions.

**Table 1**  
Adsorption isotherm constants for CR adsorption onto  $\text{Bi}_2\text{S}_3$  MSs and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs.

Adsorbent	T ( $^{\circ}\text{C}$ )	$q_{e,\text{exp}}$ ( $\text{mg g}^{-1}$ )	Langmuir isotherm constants			Freundlich isotherm constants		
			$q_m$ ( $\text{mg g}^{-1}$ )	$b$	$R^2$	$K_F$ ( $\text{mg}^{1-(1/n)} \text{L}^{1/n} \text{g}^{-1}$ )	$n$	$R^2$
$\text{Bi}_2\text{S}_3$ MSs	25	37.44	33.39	0.250	0.830	15.75	6.27	0.982
	35	48.48	41.36	0.736	0.813	22.81	7.69	0.972
	45	54.62	46.86	0.826	0.861	24.45	6.98	0.968
	55	66.28	56.27	0.912	0.890	26.91	6.08	0.980
$\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$ MSs	25	53.33	55.25	0.376	0.981	23.63	5.51	0.963
	35	72.23	70.97	0.629	0.972	28.50	4.93	0.968
	45	77.24	78.064	1.073	0.973	32.45	5.07	0.962
	55	92.24	90.580	1.302	0.987	35.72	4.79	0.958

**Table 2**  
The  $q_m$  values for the adsorption of CR on different adsorbents.

Adsorbents	$q_m$ ( $\text{mg g}^{-1}$ )	Ref.
$\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$ MSs	92.24	This study
Chitosan coated magnetic $\text{Fe}_3\text{O}_4$ particle	42.62–56.66	[56]
$\text{Fe}_{3-x}\text{La}_x\text{O}_4$ ferrite	37.4–79.1	[53]
$\text{Zn-Fe}_2\text{O}_4$	16.58	[54]
Ca-bentonite	23.25–85.29	[55]
Activated carbon	6.7	[57]

For  $\text{Bi}_2\text{S}_3$  MSs, as the initial concentration increased from  $5 \text{ mg L}^{-1}$  to  $30 \text{ mg L}^{-1}$ , the removal rate of CR decreased from 99% to 60% (Fig. 6a). However, the percentage of CR adsorption on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs reached up to 85% within 90 min for all the studied concentrations (Fig. 6b). Compared with CR adsorption process on  $\text{Bi}_2\text{S}_3$  MSs, the fast adsorption over the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs was clearly observed for all the studied concentrations. This higher efficiency and faster rate of CR adsorption on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs can be ascribed to abundant unoccupied active sites on the adsorbent's surface as well as the porous hierarchical structure of the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs [3]. On the basis of the above results, the observed high adsorption capacity and the short time needed to achieve adsorption equilibrium confirm the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs would be an effective adsorbent for CR removal.

### 3.4. Adsorption kinetics

Adsorption kinetics is one of the most important characters which govern the solute uptake rate and represent adsorption efficiency of adsorbent for design operation and optimization. To investigate adsorption kinetics of CR on  $\text{Bi}_2\text{S}_3$  MSs and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs, three different kinetic models, i.e. Lagergren-first-order model, pseudo-second-order kinetic model and intraparticle diffusion model were used to fit the adsorption kinetic data.

The Lagergren-first-order kinetic, pseudo-second-order kinetic model and intraparticle diffusion model can be given by Eqs. (5)–(7) [55].

$$\log(q_e - q_t) = \log q_e - \frac{k_1 t}{2.303} \quad (5)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \quad (6)$$

$$q_t = k_{id} t^{1/2} + c \quad (7)$$

where  $q_e$  and  $q_t$  ( $\text{mg g}^{-1}$ ) are the amounts of CR adsorbed at equilibrium and at time  $t$  (min), respectively;  $k_1$  is the rate constant of Lagergren-first-order kinetic model ( $\text{min}^{-1}$ ). Values of  $k_1$  can be calculated from the plots of  $\log(q_e - q_t)$  versus  $t$  for Eq.(5).  $k_2$  is the rate constant ( $\text{g mg}^{-1} \text{min}^{-1}$ ) of pseudo-second-order kinetic model for adsorption. The slope and intercept of the linear plots of  $t/q_t$  against

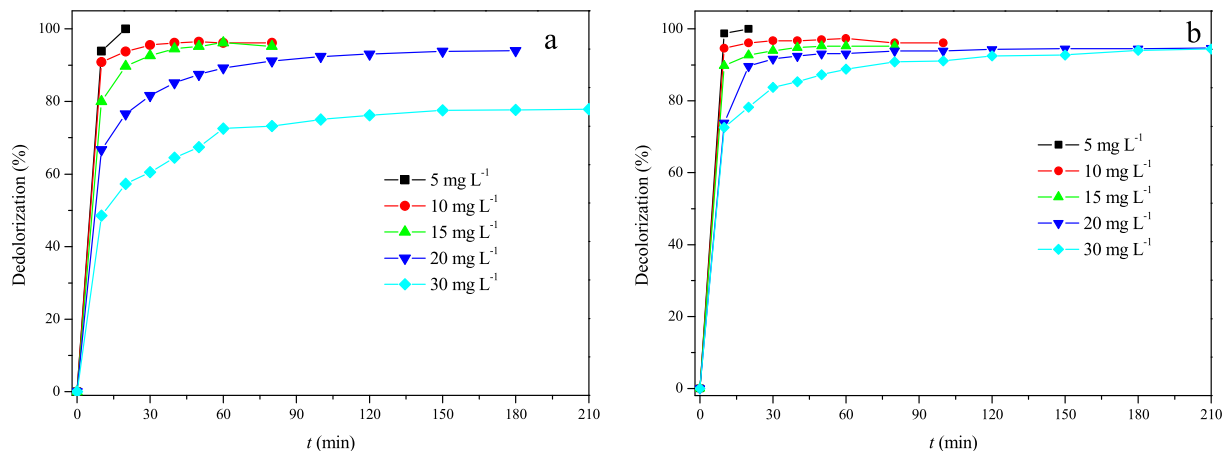


Fig. 6. CR adsorption onto  $\text{Bi}_2\text{S}_3$  microspheres (a) and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  microspheres (b) for distinct CR initial concentrations.

$t$  yield the values of  $1/q_e$  and  $1/k_2q_e^2$  for Eq. (6).  $c$  ( $\text{mg g}^{-1}$ ) is the intercept and  $k_{id}$  is the intraparticle diffusion rate constant ( $\text{mg g}^{-1} \text{min}^{-1/2}$ ), which can be calculated from the slope of the linear plots of  $q_t$  versus  $t^{1/2}$ .

Different kinetic parameters of CR adsorption onto  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs for different CR initial concentrations were shown in Table 3. The relatively low correlation coefficient ( $R^2$ ) and the large difference between the calculated value of adsorption capacity ( $q_{e,cal}$ ) and the experimental value ( $q_{e,exp}$ ) indicate that the adsorption kinetics of CR on the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs does not obey the pseudo-first-order kinetic model. However, all the experimental data showed better compliance with pseudo-second-order kinetic model in terms of higher correlation coefficient values ( $R^2 > 0.998$ ) and closer values between  $q_{e,cal}$  and  $q_{e,exp}$  (Table 3). It could be found that pseudo-second-order kinetic model was more valid to describe the adsorption behavior of CR onto  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs, indicating that the adsorption of CR on both  $\text{Bi}_2\text{S}_3$  MSs and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs are mainly controlled by chemisorption. Fig. 7 showed the regression plots of pseudo-second-order kinetic model about CR adsorption on both  $\text{Bi}_2\text{S}_3$  MSs and magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs. It was likely that the adsorption behavior may involve valence forces by sharing of electrons between anions and bio-adsorbent.

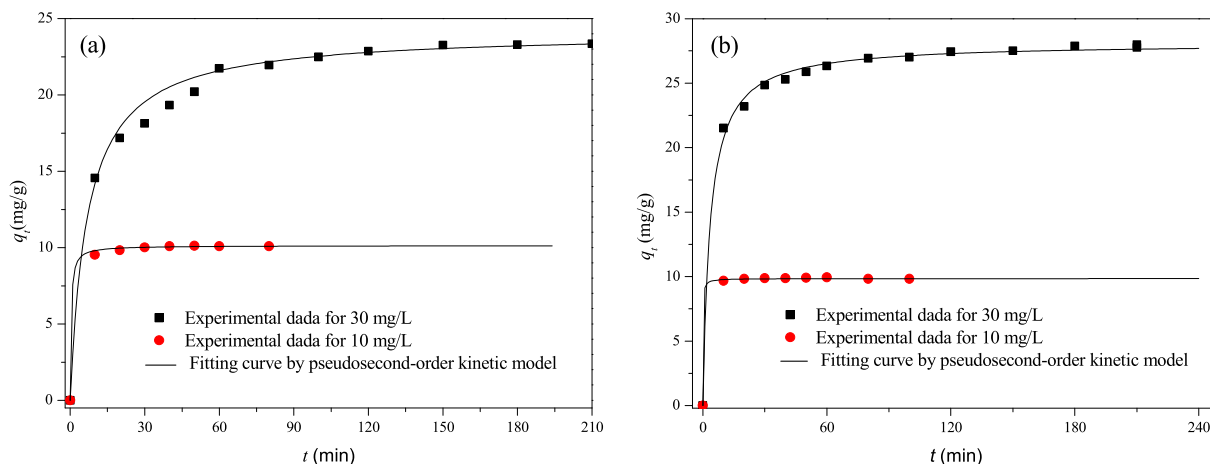
### 3.5. Photocatalytically recycling under simulated solar light

In addition to efficiency, the lifetime of water-treatment materials is also very important for practical applications. The reuse ability can be realized if  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs can self-clean CR dye molecules absorbed on it. Therefore, the reutility and stability of the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were examined through the repeated experiments based on the two different experimental procedures: (1) only adsorption in dark and (2) simultaneous adsorption and photocatalytic regeneration in one step for cycling under simulated solar light irradiation. Fig. 8 shows the successive

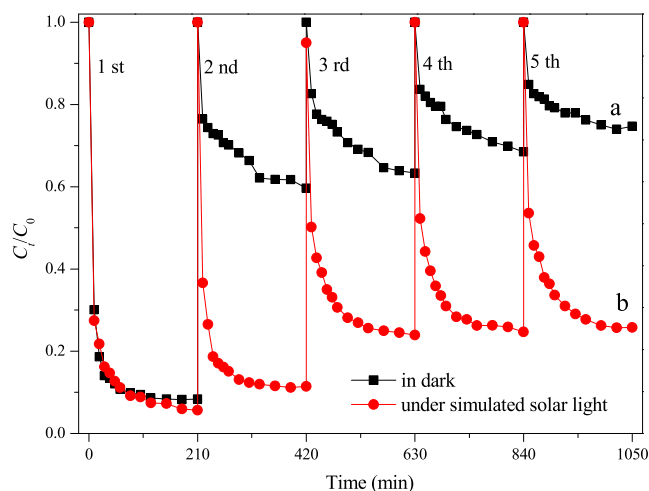
cycles of two different experimental procedures. The adsorption capacities for  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs decreased noticeably during the repeated adsorption operations. An obvious decrease from 91.60% to 40.3% in the removal efficiency was observed when the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were reused as adsorbent for the first cycle (Fig. 8 curve a). After the successive fifth cycles, the removal efficiency was only 25.3% by only adsorption in dark. The decreased efficiency after five cycles may be due to the decreased surface active sites. Interestingly, when the adsorption and photocatalytic regeneration were simultaneously performed during the repeated experiments under simulated solar light irradiation, the recyclability of the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs can be improved efficiently compared with the reuse of  $\text{Bi}_2\text{S}_3$  MSs. As shown in Fig. 8 curve b, the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs exhibited good stability and maintained high removal efficiency in successive five cycles under simulated solar light irradiation. What's more, the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs did not show a clear decrease in photodegradation efficiency after  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs were used for fifth time recycles for the decolorization of CR under simulated light irradiation. The enhanced decolorization of CR solution by  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs resulted from two main reasons. Firstly,  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs can concentrate the targeted CR dye on the surface of water-treatment materials from the diluted water to promote the CR transfer process. Secondly, CR adsorbed on the surface of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs can be photocatalytically oxidized and the adsorbent can be regenerated and reused in further cycles [27]. Several studies have shown that CR molecules can be photodecolorized by appropriated photocatalysts under light irradiation [9,58].  $\text{Bi}_2\text{S}_3$  with a typical narrow band gap can be used to photodegrade organic pollutant since  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs have a stronger absorption in the visible light area. In addition, the fact that adsorption and photocatalytic regeneration of organic compounds occur continuously in the presence of  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs avoids two independent processes and reduces the actual processing cost. As a result, magnetically recyclable  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs could be regenerated via the

Table 3  
Kinetic parameters of CR adsorption onto  $\text{Bi}_2\text{S}_3$  MSs and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSs.

Adsorbents	Con. ( $\text{mg g}^{-1}$ )	$q_{e,exp}$ ( $\text{mg g}^{-1}$ )	Lagergren-first-order model			Pseudo-second-order kinetic model			Intraparticle diffusion model		
			$q_{e,exp}$ ( $\text{mg g}^{-1}$ )	$k_1$ ( $\text{min}^{-1}$ )	$R^2$	$q_{e,exp}$ ( $\text{mg g}^{-1}$ )	$k_2$ ( $\text{mg g}^{-1} \text{min}^{-1}$ )	$R^2$	$k_i$ ( $\text{mg g}^{-1} \text{min}^{-1/2}$ )	$c$ ( $\text{mg g}^{-1}$ )	$R^2$
$\text{Bi}_2\text{S}_3$	10	10.08	5.03	0.134	0.935	10.13	0.292	1.000	0.986	3.39	0.634
	30	23.34	14.42	0.031	0.976	24.10	0.006	0.998	1.268	8.92	0.707
$\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$	10	9.81	2.10	0.097	0.760	9.84	1.321	1.000	0.778	4.15	0.531
	30	27.98	9.31	0.024	0.905	28.26	0.010	0.999	1.160	14.33	0.524



**Fig. 7.** Fitting of pseudosecond-order kinetics for CR adsorption on  $\text{Bi}_2\text{S}_3$  MSS (a) and  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSS (b). Experimental conditions: initial CR concentration  $30 \text{ mg L}^{-1}$ ; adsorbent dosage  $1.0 \text{ g L}^{-1}$

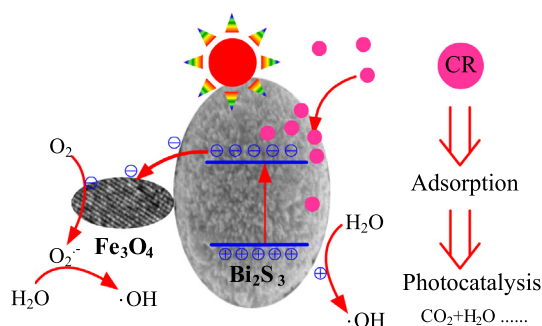


**Fig. 8.** Recycling test of the magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSS performed in dark (a) and under simulated solar light irradiation (b).

economical, green photocatalytic treatment and maintain higher processing removal efficiency of CR dye by adsorption and photocatalytic regeneration.

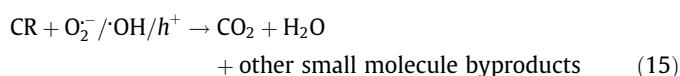
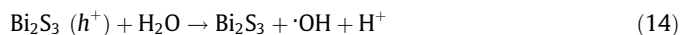
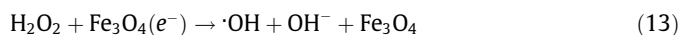
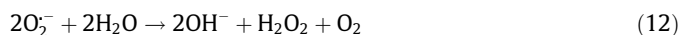
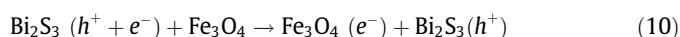
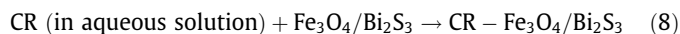
### 3.6. The possible mechanism of dye removal by $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$ MSS

As previous studies mentioned [29,46], the photodegradation of dye pollutants on photocatalyst is mainly driven by a series of reactive species including active holes ( $h^+$ ), hydroxyl radicals ( $\cdot\text{OH}$ ), and superoxide radicals ( $\text{O}_2^-$ ) generated. Based on the above experimental results and corresponding Refs. [44,46], a possible mechanism of successful CR removal by  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSS under simulated solar light irradiation was proposed as follows (Fig. 9). Firstly, CR molecules in aqueous solution were adsorbed fast onto  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSS (Eq. (8)) due to the high relative large surface areas and mesoporous channels of magnetic  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$ . At the same time, electrons ( $e^-$ ) in the valence band (VB) of  $\text{Bi}_2\text{S}_3$  in  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSS can be photoexcited to its conduction band (CB) under simulated light irradiation, causing the photoproduced holes ( $h^+$ ) in the VB of  $\text{Bi}_2\text{S}_3$  simultaneously (Eq. (9)). The CB level of  $\text{Fe}_3\text{O}_4$  (1 V vs. NHE) is much lower than that of  $\text{Bi}_2\text{S}_3$  (0.12 V vs. NHE) [22,46], so the photoproduced  $\text{Bi}_2\text{S}_3(e^-)$  may quickly migrate from conduction band of  $\text{Bi}_2\text{S}_3$  MSS into that of the  $\text{Fe}_3\text{O}_4$  and the



**Fig. 9.** Mechanism of CR removal on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSS under simulated solar light illumination.

chance of  $e^-/h^+$  recombination is greatly reduced (Eq. (10)). Following, the migrated  $e^-$  reacted with the oxygen molecule ( $\text{O}_2$ ) that dissolved in aqueous solution to yield  $\text{O}_2^-$  (Eq. (11)) [29], which further react with  $\text{H}_2\text{O}$  and to produce  $\text{H}_2\text{O}_2$  and  $\cdot\text{OH}$  (Eqs. (12) and (13)). The photoinduced holes ( $h^+$ ) at the VB top of  $\text{Bi}_2\text{S}_3$  with potential of about 2.07 eV [31], which is more positive than the standard reduction potential of  $\text{OH}^-/\cdot\text{OH}$  (1.99 eV), can react with  $\text{H}_2\text{O}$  to produce  $\cdot\text{OH}$  radicals (Eq. (14)). At last, all the produced active species including  $\cdot\text{OH}$ ,  $e^-/h^+$  and  $\text{O}_2^-$  can attacked the N=N bonds of CR molecules adsorbed on  $\text{Fe}_3\text{O}_4/\text{Bi}_2\text{S}_3$  MSS and further oxidize the broken CR molecules into  $\text{CO}_2$ ,  $\text{H}_2\text{O}$  and other small molecule byproducts (Eq. (15)) [29].





#### 4. Conclusions

In summary, magnetically recyclable Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs combining the highly effective adsorption and green photocatalytic regeneration were prepared by a facile hydrothermal method. The as-obtained Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs possessed a relative high surface area, low coercivity value and remanent magnetization value. The Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs can be easily and economically separated, regenerated and re-dispersed in aqueous solution, which is desirable for practical application. The equilibrium and kinetics of adsorption process followed the Langmuir isotherm model and pseudo-second-order kinetic for CR adsorption on Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs, respectively. The maximum adsorption capacity of CR for Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs as 92.24 mg g<sup>-1</sup> was achieved by Langmuir isotherm model, while only 66.28 mg g<sup>-1</sup> was found for Bi<sub>2</sub>S<sub>3</sub> MSs. Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs also show excellent stability and reusability for effective removal of Congo red dye by simultaneous adsorption and photocatalytic regeneration. As a result, Fe<sub>3</sub>O<sub>4</sub>/Bi<sub>2</sub>S<sub>3</sub> MSs provide effective and conveniently recyclable materials for the environmental remediation and purification of wastewater by providing the facile preparation, easy magnetic separation, high adsorption, and simple regeneration.

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