

# 2,4-DINITROTOLUENE REMOVAL EFFICIENCY AND MECHANISMS IN TREATMENT OF CHEMICAL INDUSTRIAL WASTEWATER WITH ZERO-VALENT FE/CU BIMETAL

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#### ABSTRACT

Driven by chemical substitution, Fe/Cu bimetal materials were developed through copper sedimentation on iron crumbs, and characterized through a scanning electron microscope (SEM) and X-ray electron spectrometers. Fe/Cu bimetal were used in the treatment of systems 2,4-dinitrotoluene (2,4-DNT) chemical industrial wastewater, whilst the research was made on treatment efficiency and reaction rate based upon respective factors ranging from the materials, coverage rate of copper, pH and initial concentration, etc. which led us into the discussion of inner mechanisms. It was demonstrated that the best coverage rate of copper plating is 0.25%, and that Fe/Cu bimetal materials supersede simple iron crumbs regarding removal efficiency, reaction rate and adaptation. With pH set at 9.0, 11.0 and 13.0, the removal of 2,4-dinitrotoluene increased by 6.22%, 9.52% and 25.26%, changing from iron crumbs to Fe/Cu bimetal, reaching at 90.18%, 70.21% and 58.8% respectively. Fe/Cu bimetal material tackles the low degradation efficiency in alkaline environments faced by conventional micro-electrolysis and is not limited within acidic wastewater treatment.

#### Key Words:

Iron Crumb; Fe/Cu Bimetal; 2,4–DNT; Chemical Industrial Wastewater

# **INTRODUCTION**

2,4-dinitrotoluene (2,4-DNT) is a type of widely used material in chemical industry, and an intermediate in fine chemicals, with strong bio-toxicity and 'three causing' effects, namely causing cancer, causing malformation and causing mutation. Once into water bodies, it aggravates the quality and sensory properties of the water for long terms, and brings about great hazards to the environment and organisms. It has been listed in the '58 chemicals prioritized for control' in China for environmental protection (Ma et al.2013; Zhang et al). Due to the fact that these chemicals are highly stable in water bodies, conventional wastewater treatment could barely degrade and remove them from water bodies. Physical-chemical treatment, combined with bio-chemical treatment, is currently the dominant technique in the treatment of DNT chemical industrial wastewater both domestically and abroad.

In the process of treating DNT chemical industrial wastewater, a critical and restrictive step is bringing down the concentration of DNT and the toxicity of the wastewater before bio-chemical treatment. The research so far has been founded on oxidation techniques, e.g. electrochemical oxidation, Fenton oxidation and photo-catalytic oxidation. These oxidation techniques are universally too costly, making it an urgent need to find a low cost and effective way to treat DNT chemical industrial wastewater (Bozzi et al, 2005; Ma et al, 2008).

micro-electrolysis, Iron-carbon using reduction, absorption, flocculation and filtration for pollutant removal, has developed along with the utilization of iron in wastewater treatment, and is more economical compared with oxidation (Jiang et al, 2009). However, after a certain time period of running, the iron crumbs harden up and short circuits are formed; meanwhile, it's only performing well under acidic conditions (Ma et al, 2008; Wang et al, 2009; B et al, 2014). Targeting at the deficiencies above, Chen used discarded iron shavings as a base matter and fabricated bimetal reduction systems such as Cu/Fe, and carried out a research on fine chemicals industrial wastewater and dyeing wastewater (Chen et al, 2011). Compared with conventional iron-carbon micro-electrolysis, bimetal systems have a wider suitable pH range (e.g. from the acidic environment to slight alkaline environment) for a good effectiveness, along with improvements in iron crumb hardening up (Ma et al, 2004). However, regarding whether Fe/Cu bimetal is suitable for

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DNT chemical industrial wastewater, or the effectiveness and reaction mechanisms, we have noticed barely any report by far. This led us to use iron crumbs as the base matter and build Fe/Cu bimetal systems for the treatment of DNT chemical industrial wastewater, and made a research on treatment efficiency and reaction rate based upon respective factors ranging from the materials, coverage rate of copper, pH and initial concentration etc. We optimized the conditions of the reaction systems, aiming at offering some certain reference to the practical utilization of Fe/Cu bimetal systems in the treatment of nitro-containing aromatic compounds chemical industrial wastewater.

#### MATERIALS AND METHODS

# **REAGENTS AND INSTRUMENTS**

The 0.1 cm diameter iron crumbs were obtained from a machinery plant in Linhai, Zhejiang Province. Chemicals used are graded AR (analytical reagent). Instruments used in the experiment include DELTA-320 pH meter (DELTA, China), UV-7504 (A) ultraviolet visible spectrophotometer(Metash, China), KYC-1102C air thermostatic table(KYC, China), D8 advance X-ray diffractometer (Bruker, German), Specific surface and pore size analyzer (Beishide Instrument, china), and Hitachi S-4800 scanning electron microscopy (Tokyo, Japan).

# FABRICATION AND CHARACTERIZATION

#### Fabrication of Fe/Cu Bimetal.

(1)Pretreatment: Soak the discarded iron crumbs from the machinery plant with 10% alkali for 5-10 min to remove attached grease, and then with 3% HCl for 30 min to remove the oxide on the surface, and then cleaned with water.

(2)Place 100g pre-treated iron scraps respectiv ely into each of three containers of 1000mL volume , followed by dosing in 400mL distilled water. Then dose CuSO4 solution of 1 g/L concentration into th e three containers by 100mL, 250mL and 500mL re spectively, which leads to Fe/Cu bimetal with a cop per rate of 0.1wt%, 0.25wt% an 0.5wt% respectivel y.

**Characterization**. Micro-morphology analysis and Energy Dispersive Spectrometer analysis for the catalysts were carried out with a Hitachi S-4800 scanning electron microscopy (SEM). A Bruker AXS D8 Advance X-ray diffractometer (XRD) was used for X-ray diffraction, and the Specific surface of the iron scraps was tested to be 0.2045m<sup>2</sup>/g on a Specific surface and pore size analyzer(Beishide Instrument 3H-2000PS2).

#### METHODS

The prepared materials was put in a packed-bed reactor with an effective volume of 0.5 L as the packing. The packed-bed reactor is about 250mm high and 50 mm in diameter.2,4–DNT chemical industrial wastewater flowed into the upflow packed-bed reactor at room temperature( $20\pm3^{\circ}$ C), and the upflow rate was 0.1 m/h. Samples were taken regularly from 0 to 2 h for analysis ,and a series of data was obtained as the condition factors were altered. Reduction-azo spectrophotometry was adopted for determining the concentration of nitrobenzene, and phenanthroline spectrophotometry for gross iron ion concentration.

#### **RESULTS AND DISCUSSION**

# CHARACTERIZATION

**Scanning Electron Micrographs (SEM).** As shown in Fig. 1, the surface of iron crumbs is relatively smooth and compact, without too many openings or cracks, whilst the surface of Cu/Fe bimetal is rough with many particles, indicating a micro-morphology change of the iron crumbs when covered with copper.

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(a) SEM Image of Iron Crumbs



(b) SEM Images of Cu/Fe Bimetal

# FIGURE 1 SEM Images.

X-ray Energy Dispersive Spectroscopy (EDS) Image. Fig. 2 shows X-ray EDS images of iron crumbs and Cu/Fe bimetal of 0.25% copper rate. Table 1 shows the results element contents) of the samples. EDS image of the iron crumbs shows Fe and C as the predominant elements, taking up 79.91% and 18.22% of weight percentage respectively. EDS image of Cu/Fe bimetal shows the existence of Cu, Fe, C and O, indicating that Cu/Fe bimetal has been created as the iron crumbs were coppered. It's also seen that the atomic percentage of O is only 9.43%, whilst Fe and Cu takes 18.69% of atomic percentage, which indicates that during the fabrication of the materials, just a part of the zero-valent elements were oxidized, and that zero-valent Cu/Fe systems still exist in the Cu/Fe bimetal materials.



# FIGURE 2 EDS Images.

 TABLE 1

 Element Analysis EDS Images of Iron Crumbs and Cu/Fe Bimetal

Material	Iron Crumbs				Cu/Fe Bimetal			
Element	С	Si	Fe	-	С	0	Fe	Cu
Weight percentage	18.22	1.87	79.91	-	40.09	7.01	16.50	36.40
Atomic percentage	46.30	2.04	51.68	-	71.87	9.43	6.36	12.33

RESEARCHES INTO INFLUENTIAL FACTORS

**Effects of Copper Rate.** The prepared materials was put in a packed-bed reactor with an effective volume of 0.5 L as the packing. Put into

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each of four 500 mL sized small packed-bed reactors 100g of iron crumbs, the copper rate of which being respectively 0%, 0.1wt%, 0.25wt% and 0.5wt%. Put in 2,4–DNT wastewater of 100

mg/L in concentration and 7 in pH. To have the materials fully blended, and samples were taken regularly from 0 to 2h for determination. See Fig. 3 for the outcomes.



FIGURE 3 Effects of Copper Rate on Removal Rate.

As shown in Fig. 3, after 15 min of reaction, the degradation rate of DNT in relation to iron crumbs with no copper was 78.41%, and 80%, 85%, 75.9% respectively as copper rate goes up to 0.1wt%, 0.25wt% and 0.5wt%, which indicates that from 0 to 0.25wt%, the degradation efficiency and reaction rate improves as Fe/Cu bimetal systems are established, yet when copper rate goes up to 0.5wt%, degradation rate drops.

Wu et al. (Wu et al, 2005) were convinced that the existence of copper in Fe/Cu bimetal systems accelerates primary battery reactions, and makes reduction reactions easier for organics on the surface of iron and copper due to the unique inner metal-crystal structure and electron arrays, which is in line with the outcomes of this experiment within a copper rate range of 0 to 0.25 wt%. The fact that removal rate drops significantly as copper rate reaches 0.5 wt% has led us to believe that as copper rate increases to a certain degree, iron as the anode of the primary battery is covered bytoo much copper, which diminishes the direct contact area of iron with 2,4-DNT in the wastewater, and thus hinders electrons from being transferred from the iron anode, which is an obstacle for the reduction reactions and brings down reaction rate and treatment effectiveness. In accordance with the outcomes of this experiment, the optimized copper rate on iron crumbs is 0.25wt%.

**Effects of pH**. Put into each of 12 small packed-bed reactors 100 g of iron crumbs without copper or Fe/Cu bimetal with a copper rate of 0.25wt%. Put in 2,4–DNT wastewater of 100 mg/L in concentration and change the pH with HCl or NaOH solution to 3.0, 5.0, 7.0, 9.0, 11.0 and 13.0, respectively. To have the materials fully blended, the reactor was placed in the air thermostatic table for shaking, and samples were taken regularly from 0 to 2 h for determination. See Fig. 4 for the outcomes.



(a) Effects of pH for Iron Crumbs on Removal Rate (b) Effects of pH for Fe/Cu Bimetal on Removal Rate

FIGURE 4 Effects of pH.

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As shown in Fig. 4, after 2 h of reaction, the degradation rate of 2,4-DNT in relation to iron crumbs with no copper was around 95% at pH of 3.0, 5.0 and 7.0, and 83.96%, 59.25%, 33.54%, respectively as pH goes up to 9.0, 11.0 and 13.0, which indicates that from pH 9 to pH 13, the removal rate of DNT significantly drops as pH goes up. It's also seen that after 2 h of reaction, the degradation rate of 2,4-DNT in relation to Fe/Cu bimetal (copper rate 0.25wt%) was around 98% at pH of 3.0, 5.0 and 7.0, and 90.18%, 70.21%, 58.8% respectively as pH goes up to 9.0, 11.0 and 13.0.

Comparing iron crumbs without copper and Fe/Cu bimetal, we can see that at pH of 3.0, 5.0 and 7.0, both could give a satisfying removal rate above 95% on DNT, yet Fe/Cu bimetal is better at pH of 9.0, 11.0 and 13.0, respectively 6.22%, 9.52% and 25.26% higher compared to iron crumbs, which indicates that as alkalinity increases, Fe/Cu bimetal

is better than iron crumbs. The results imply that to a certain degree, Fe/Cu bimetal material tackles the low degradation efficiency in alkaline environments faced by conventional micro-electrolysis and is not limited within acidic wastewater treatment. According to the literature(Wu et al,2009;Su et al,2012;Chang et al,2010), there are two predominant reduction reactions going on in the reaction system of the experiment, one being the direct reduction effects of zero-valence iron, another being the reduction effects of newly generated [H] (B. Lai ,et al.2014).

**Effects of Concentration**. Put into packed-bed reactors filled with Fe/Cu bimetal (copper rate 0.25%) 2,4–DNT wastewater of pH 7 and different concentrations. Samples were taken regularly for determination. See Fig. 5 for the outcomes.



FIGURE 5 Effects of Concentration for Fe/Cu Bimetal (Copper Rate 0.25%) on Removal Rate.

As shown in Fig. 5, the degradation efficiency of 2,4-DNT in the packed-bed reactor filled with Fe/Cu bimetal does not change much as the initial concentration of 2,4-DNT increases from 50 mg/L to 200 mg/L and stays around 98%. As inlet concentration increased up to 400 mg/L, it drops to 88.15%. These outcomes indicate that packed-bed reactors filled with Fe/Cu bimetal is adaptable to the change of 2,4-DNT inlet concentration to some extent, yet when the concentration goes up to some degree, remove rate is suppressed(Fan et al,2009;Zhu et al,2013). A higher initial pollutant concentration would lead to competitive adsorption among the pollutant and its intermediates because the adsorption reaction area of Fe/Cu is fixed. The competitive adsorption would affect the mass-transfer rate of the pollutant and its intermediates between the solution and the surface of Fe/Cu, which would become a limiting factor when the initial concentration was much higher (Y. Yuan et al.2014).

# A RESEARCH INTO REACTION KINETICS

This paper studies the reaction kinetics of 2,4-DNT wastewater treatment by iron crumbs or Fe/Cu bimetal with the first-order reaction kinetic equation  $dC/dt=-K_{obs}\bullet C$ , and the results are as shown in Table 2 and Fig. 6. Kinetic equations in Table 2 reflect a linear relationship between  $ln(C/C_0)$  and t (time), with a noticeable linear regression coefficient R<sup>2</sup>, which demonstrates well the kinetic characteristics of first-order reactions. As shown in Fig. 6, the reaction rate of 2,4-DNT degradation by Fe/Cu bimetal is higher than that of iron crumbs under all pH conditions, implying that the fabrication of Fe/Cu bimetal systems does a good job in accelerating the reaction rate.

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# RESEARCH INTO REACTION MECHANISMS

**Researches into Process Products in Reaction.** Put into packed-bed reactors filled with Fe/Cu bimetal (copper rate 0.25%) 2,4–DNT wastewater of pH 7 and 100mg/L in concentration. Samples were taken regularly for ultraviolet spectrum scanning analysis, Fig. 7 for the outcomes of UV spectrum scanning. As shown in Fig. 7, the absorption peak at 250nm wavelength gets weaker and weaker as the reaction goes on, and disappears at 120min; at the same time, the absorption peak at 215nm wavelength gets stronger gradually and reaches the highest at 120min. Based on the analysis of UV spectrum scanning outcomes, 2,4-DNT gets mostly degraded, whilst new matters are generated in the reactions.

 TABLE 2

 Kinetic Parameters of 2,4-DNT Degradation by Iron Crumbs and Fe/Cu Bimetal.

	Iron Filings	Vinctics Equation	Fe/Cu	Kinetics Equation	
рн –	R <sup>2</sup>	- Killetics Equation	R <sup>2</sup>		
3	0.93475	ln(C <sub>t</sub> /C <sub>0</sub> )=-(0.75867+0.02547t)	0.91279	ln(C <sub>t</sub> /C <sub>0</sub> )=-(1.09236+0.03085t)	
5	0.90945	ln(C <sub>t</sub> /C <sub>0</sub> )=-(0.80302+0.02261t)	0.906	ln(C <sub>t</sub> /C <sub>0</sub> )=-( 1.05759+0.02831t)	
7	0.9134	ln(C <sub>t</sub> /C <sub>0</sub> )=-( 0.76094+0.0217t)	0.88546	ln(C <sub>t</sub> /C <sub>0</sub> )=-( 1.07656+0.02608t)	
9	0.86273	ln(C <sub>t</sub> /C <sub>0</sub> )=-(0.55985+0.01327t)	0.89118	In(C <sub>t</sub> /C <sub>0</sub> )=-(0.64426+0.01679t)	
11	0.78711	ln(C <sub>t</sub> /C <sub>0</sub> )=-(0.35469+0.00571t)	0.81592	ln(C <sub>t</sub> /C <sub>0</sub> )=-(0.44627+0.008t)	
13	0.92083	In(C <sub>t</sub> /C <sub>0</sub> )=-(0.08466+0.00328t)	0.86297	In(C <sub>t</sub> /C <sub>0</sub> )=-(0.28086+0.00622t)	



Reaction Rate of 2,4-DNT Degradation by Iron Crumbs and Fe/Cu Bimetal.



FIGURE 7 Ultraviolet Spectrum Scanning Graphs of Cu/Fe.

**Variations of pH and Iron Ion Concentration.** As shown in Fig. 8, during the treatment of 2,4-DNT wastewater by Fe/Cu bimetal, pH increases as the reaction goes on but not significantly, remaining between 7 - 8. At the starting period, stripping of iron ions is observed, reaching 1.23mg/L, and drops to 0.52mg/L as the reaction goes on, and fluctuates between 0.68mg/L and 0.86mg/L afterwards. It is believed that during redox reactions, electrons are lost from iron atoms, generating iron ions in the solution. Meanwhile, some H+ are consumed, leading to pH increase, and thus Fe(OH)2 is generated as iron ions are combined with OH-, leading to the decrease of iron ion concentration in the system and pH maintaining between 7-8(Scherer et al.2001;Liu et al.2005).



FIGURE 8 Variation of pH and Iron Ion Concentration.

**Discussion on Reaction Mechanisms.** In accordance with a research into the phenomenon of the experiment in this paper, the mechanisms of DNT wastewater treatment by zero-valence Fe/Cu bimetal could be approached from four perspectives, namely (1) direct electron transfer on the surface of

Fe/Cu bimetal, (2) micro primary battery effects, (3) the effects of bimetal, and (4) adsorption of the corrosion products of Fe<sup>0</sup> (Xu et al.2008; Liang et al.2010].

(1) Direct electron transfer on the surface of Fe/Cu bimetal.



#### (2) Micro primary battery effects.

 $E (Fe^{2^+}/Fe) = -0.44V$ Anode (Fe): Fe–2e $\rightarrow$ Fe<sup>2+</sup> Cathode (C):  $2H^++2e \rightarrow 2[H] \rightarrow H_2$  $E (H^{+}/H_{2}) = 0V$ Cathode reactions are as follows with the existence of oxygen:  $O_2+4H^++4e \rightarrow 2H_2O$ E(O<sub>2</sub>)=1.23V  $O_2+2H_2O+4e\rightarrow 4OH^-$ E(O<sub>2</sub>/OH<sup>-</sup>)=0.41V CH<sub>3</sub> CH<sub>3</sub> NO<sub>2</sub> NH<sub>2</sub> 12[H] + $+4H_2O$ NO<sub>2</sub> ΝH<sub>2</sub>

(3) Effects of bimetal. In the bimetal system of copper and iron, copper as the cathode improves the reaction rate of the micro primary battery, and also provides a reaction surface for the reduction reactions of DNT, which enhances the reaction rate of the system (Liang et al.2010).



(4) Adsorption of the corrosion products of  $Fe^{0}$ . The removal of DNT also was resulted from the adsorption of the corrosion products of  $Fe^{0}$ .

# CONCLUSIONS

(1) The optimized copper rate on iron crumbs is 0.25%. With pH set at 9.0, 11.0 and 13.0, the removal rate increased by 6.22%, 9.52% and 25.26% changing from iron crumbs to Fe/Cu bimetal, reaching at 90.18%, 70.21% and 58.8% respectively. Fe/Cu bimetal material tackles the low degradation efficiency in alkaline environments faced by conventional micro-electrolysis and is not limited within acidic wastewater treatment.

(2) The reaction rate of 2,4-DNT degradation by Fe/Cu bimetal is higher than that of iron crumbs under all pH conditions, implying that the fabrication of Fe/Cu bimetal systems does a good job in accelerating the reaction rate.

(3) The mechanisms of DNT wastewater treatment by zero-valence Fe/Cu bimetal could be approached from three perspectives, namely (1) direct electron transfer on the surface of Fe/Cu bimetal, (2) micro primary battery effects, and (3) the effects of bimetal.

#### ACKNOWLEDGEMENTS

This work was financially supported by Public Technology Applied Research Fund of Zhejiang Province Science and Technology Department (2013C33020), Environmental Science and Technology Project of Zhejiang Province (2013B018), Priority Academic Program Development of Jiangsu Higher Education Institutions and Research Fund for Plant Evolutionary Ecology Innovative Research Team.

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<b>Received:</b>	12.07.2015
Accepted:	09.12.2015

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